

Module 6: Physical Processes in Rivers and Lakes

Principles of Surface Water Quality Modeling and Control. R.V. Thomann and J.A. Mueller. Harper & Row, New York. 1987.

Chemical Fate and Transport in the Environment, 2nd edition. H.F. Hemond and E.J. Fechner-Levy. Academic Press. London. 2000.

Physical Processes in Rivers

Fickian Mixing Processes

- A mass of chemical released in a river will spread out as it moves downstream.
- This dispersion is caused by the velocity shear within the river, and turbulent diffusion.
- Water moves more rapidly down the center of the channel, near the surface, transporting chemicals faster, and elongating the “plume.”
- Plots of concentration vs. distance has the shape of a Gaussian (normal) curve:

$$\phi(x) = \frac{1}{\sigma\sqrt{2\pi}} e^{-x^2/2\sigma^2}$$

- For a pulse injection, there is a close relationship between a Fickian mixing, or transport, coefficient D in a given direction and the standard deviation of the chemical distribution in that direction.
- D can be calculated from: $D = \sigma^2/2t$
where σ^2 is the spatial variance (the square of the standard deviation) and t is the time since the injection.
- The concentration of a conservative tracer (C) at any time (t) after injection and any distance (x) downstream is:

$$C(x,t) = \frac{M}{\sqrt{4\pi D_L t}} e^{-(x-Vt)^2/(4D_L t)}$$

Where D_L is the longitudinal Fickian mixing coefficient [L^2/T]

River	Depth (m)	Width (m)	Velocity (m/sec)	Longitudinal dispersion coefficient (m ² /sec)
Irrigation canal	0.14	1.5	0.33	1.9
Monocacy	0.32	35	0.21	4.7
Monocacy	0.45	37	0.32	13.9
Monocacy	0.88	48	0.44	37.2
Yadkin	2.33	70	0.43	111
Yadkin	3.85	72	0.76	260
Susquehanna	1.35	203	0.39	92.9
Sabine	2.04	104	0.58	316
Sabine	4.75	128	0.64	670
Missouri	2.70	200	1.55	1500

Hemond and Fechner-Levy 2000

- If the chemical undergoes a first-order decay, then the following predicts downstream concentrations:

$$C(x, t) = \frac{M}{\sqrt{4\pi D_L t}} e^{-(x-Vt)^2 / (4D_L t)} \bullet e^{-kt}$$

At any given time t, the maximum concentration of the chemical (C_{\max}) is found using:

$$C_{\max} = \frac{M}{\sqrt{4\pi D_L t}} \bullet e^{-kt}$$

- If the chemical is not instantaneously mixed across the river, a "mixing" zone is created. The chemical must travel a certain distance before the chemical is uniform across the channel.
- The lateral standard deviation of the chemical's concentration distribution can be estimated when this value is approximately equal to the river width (w):

$$\sigma_t = \sqrt{2D_t t} \approx w$$

Substituting the earlier expression for travel time, t, results in the following equation that can be used to predict the length of the transverse mixing zone:

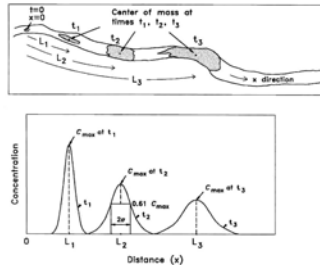
$$L \approx \frac{w^2 V}{2D_t}$$

River type/river	Transverse dispersion coefficients (m ² /sec)	Discharge during dispersion measurement (m ³ /sec)
Straight channels		
Atrisco	0.010	7.4
South	0.0047	1.5
Athabasca	0.093	776
Bends		
Missouri	1.1	1900 ^b
Beaver	0.043	20.5
Mississippi	0.1	92–120
Meandering		
Missouri	0.12	966
Danube	0.038	1030
Rea	0.0014	0.30
Orinoco	3.1	47,000
MacKenzie	0.67	15,000 ^b

Hemond and Fechner-Levy 2000

Example Problem 2-2

- The dye concentration profile was measured at time 2 in the dye transport plot, 5 hours after injection. What is the average river velocity if the max. concentration is occurring 1025 m down river from the injection location?



The velocity of the dye from the injection location to the time 2 location is:

$$V = \frac{L_2}{t_2} = \frac{1025m}{5hr} = 205m/hr$$

Estimate the longitudinal dispersion coefficient for this river if the standard deviation, σ_L , in the longitudinal direction is approx. 350 m when the chemical has traveled a distance of 1975 m to L_3

The travel time to this location is:

$$\tau_3 = \frac{L_3}{V} = \frac{1975m}{205m/hr} = 9.6hr$$

The longitudinal dispersion coefficient, D_L , can then be estimated:

$$D_L = \sigma_L^2 / 2\tau = (350m)^2 / (2 \cdot 9.6hr) \approx 6400m^2/hr$$

Estimates of Fickian Transport Coefficients from Flow Data

- Turbulence is caused by velocity shear due to a nonuniform velocity profile. The shear velocity (related to the shear force per unit area) can be estimated:

$$u^* = \sqrt{gdS} \quad \text{Where } d \text{ is the stream depth and } S \text{ is the slope}$$

This shear velocity can be used to estimate the transverse dispersion coefficient, D_t :

$$D_t \approx 0.15 \cdot d \cdot u^* \quad \text{For straight channels}$$

$$D_t \approx 0.6 \cdot d \cdot u^* \quad \text{For typical natural channels}$$

The following equation can be used to predict the longitudinal dispersion coefficient, D_L :

$$D_L = \frac{0.011 \cdot V^2 \cdot w^2}{d \cdot u^*}$$

Where V is the average velocity [L/T]
w is the stream width [L]
d is the stream depth [L]

Example Design for a Dye Injection Experiment for the Cahaba River

Solve the instantaneous equation for M to determine the amount of conservative dye to be used:

$$C(x,t) = \frac{M}{2A\sqrt{4\pi D_L t}} e^{-(x-Vt)^2/(4D_L t)}$$

- 1) Estimate the average velocity (V) and travel time (t) to the location of interest (x), and determine the corresponding desired dye concentration (C) at that location.
- 2) Estimate the longitudinal dispersion coefficient, D_L .
- 3) Solve for M, the needed mass of dye to be instantaneously released.

1) Estimate the average velocity (V) and travel time (t) to the location of interest (x), and determine the corresponding desired dye concentration (C) at that location.

- The monitoring location is 4 miles from the discharge location (x = 4 miles, 21,120 ft).
- The mean flow for the Cahaba River in this area is 99 MGD, the average width is 30 ft, and the average depth is 1.7 ft.
- The average velocity in this reach is therefore expected to be 3 ft/sec (V=3 ft/sec).
- The travel time is therefore 2 hours (0.08 days)
- The desired dye concentration at the location 4 miles from the discharge location is 250 ppb (v/v).

2) Estimate the longitudinal dispersion coefficient, D_L .

$$D_L = \frac{0.011 \cdot V^2 \cdot w^2}{d \cdot u^*} \quad u^* = \sqrt{gdS}$$

$$g = 32.2 \text{ ft/sec}^2$$

$$d = 1.7 \text{ ft}$$

$$S = 0.01$$

$$V = 3 \text{ ft/sec}$$

$$w = 30 \text{ ft}$$

Therefore,

$$u^* = 0.74 \text{ ft/sec}$$

$$D_L = 71 \text{ ft}^2/\text{sec}$$

3) Solve for M, the needed mass of dye to be instantaneously released.

$$M = \frac{2AC\sqrt{4\pi D_L t}}{e^{-(x-Vt)^2/(4D_L t)}}$$

$C = 250 \text{ ppb} = 250/1,000,000,000 = 2.5 \times 10^{-7}$

$D_L = 71 \text{ ft}^2/\text{sec}$

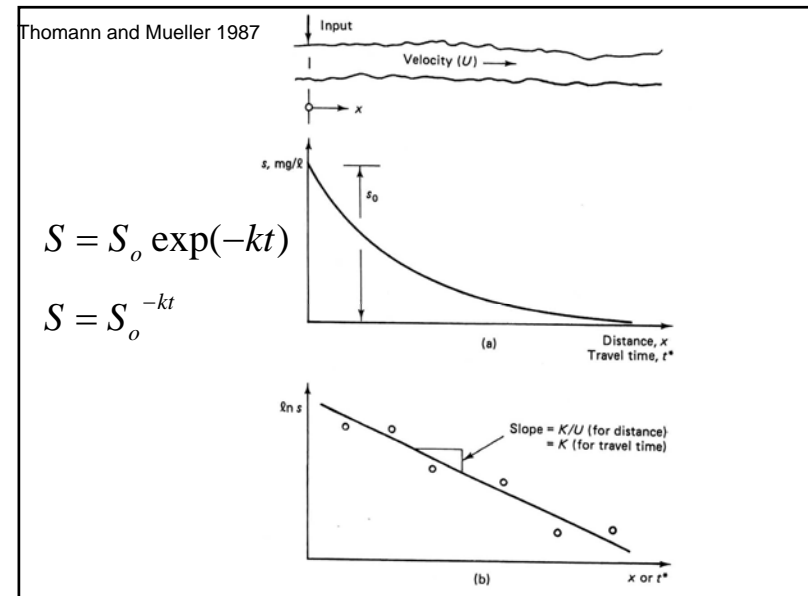
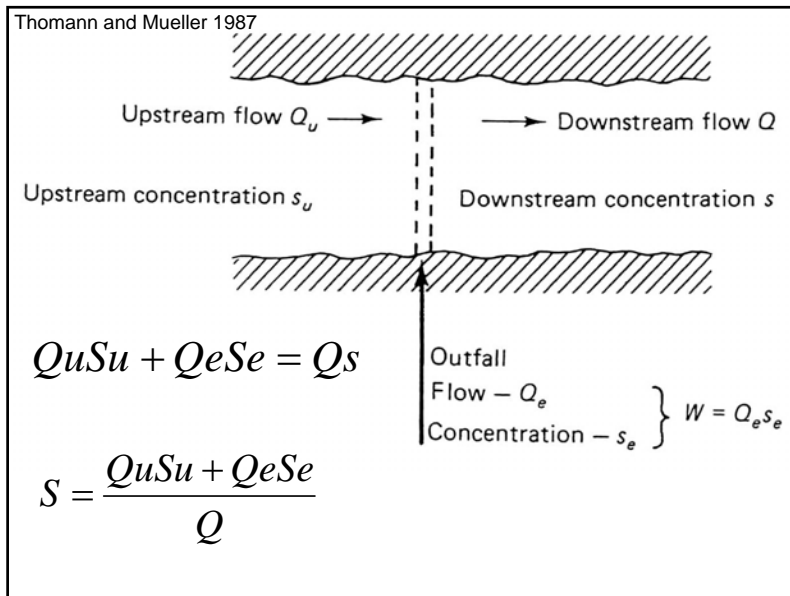
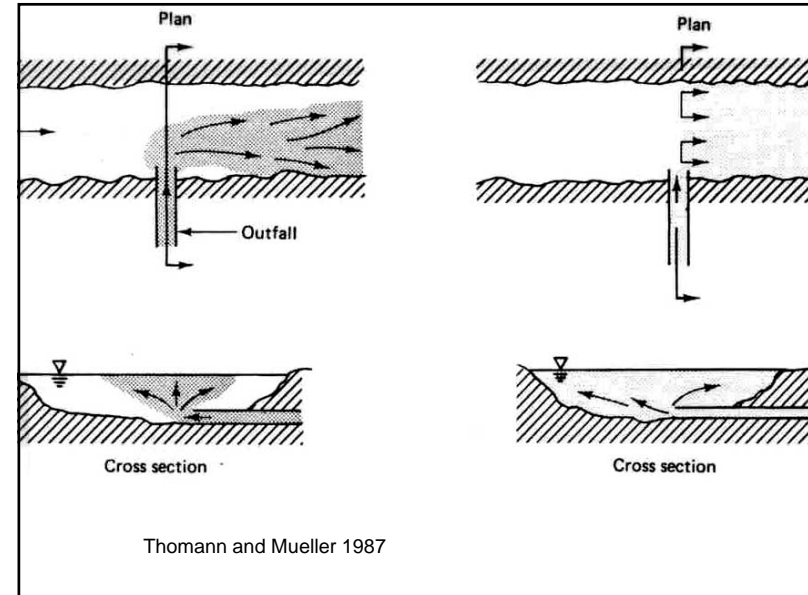
$t = 7,040 \text{ sec}$

$x = 21,120 \text{ ft}$

$V = 3 \text{ ft/sec}$

$A = 51 \text{ ft}^2$

Therefore, $M = 0.032 \text{ ft}^3$, or 0.24 gal (about 1 L)



Example Problem

- Upstream flow is 50 cfs no background concentration of pollutant
- Discharge is 10 MGD at 100 mg/L ($k = 0.1/\text{day}$)
- River velocity is 5 miles/day
- What is the concentration at 10 miles downstream?
- How much reduction is needed if the 10 mi conc. must be $< 15 \text{ mg/L}$?

$$Q_e = \frac{10 \times 10^6 \text{ gal}}{\text{day}} \times \frac{\text{ft}^3}{7.48 \text{ gal}} \times \frac{\text{day}}{86,400 \text{ sec}} = 15.5 \text{ ft}^3 / \text{sec}$$

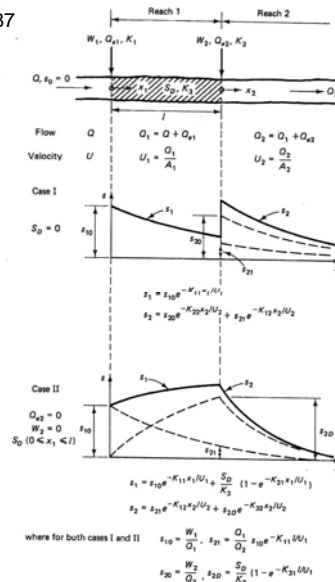
$$Q = 50 + 15.5 \text{ cfs} = 65.5 \text{ cfs}$$

$$S_o = \left(\frac{15.5 \text{ cfs}}{65.5 \text{ cfs}} \right) 100 \text{ mg} / \text{L} = 23.66 \text{ mg} / \text{L}$$

$$S = S_o \exp(-kt) = (23.66 \text{ mg} / \text{L}) \exp\left(\frac{-(0.1/\text{day})(10 \text{ mi})}{5 \text{ mi} / \text{day}} \right) = 19.4 \text{ mg} / \text{L}$$

$$\left(\frac{19.4 - 15}{19.4} \right) 100 = 23\% \text{ reduction}$$

Thomann and Mueller 1987



Physical Processes in Lakes

Fickian Mixing in Lakes

- A mass of tracer injected into a lake will move by advection with the water currents, but will also spread out into an ever-larger volume of water.
- Given enough time, it will tend to become completely mixed.
- This mixing is primarily due to turbulence, carrying chemicals away from regions of higher concentrations to areas of lower concentrations.

- Concentrations for an instantaneous discharge into a two-dimensional body of water (vertically mixed):

$$C(x, y, t) = \frac{M}{4\pi t \sqrt{D_x D_y}} e^{-((x-V_x t)^2 / (4D_x t) + (y-V_y t)^2 / (4D_y t))} \bullet e^{-kt}$$

M is the mass of the chemical discharged, per depth of water [M/L]

x and y are the distances from the injection location [L]

t is the time lapsed since injection [T]

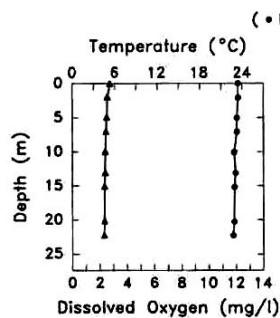
V_x and V_y are the average velocity in the x and y directions [L/T]

D_x and D_y are the Fickian transport coefficients in the x and y directions [L²/T]

K is the first-order decay rate constant [T⁻¹]

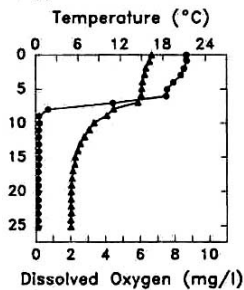
The depth is the total depth for a vertically well-mixed lake, or the thickness of a layer in a stratified lake.

Hemond and Fechner-Levy 2000
Spring

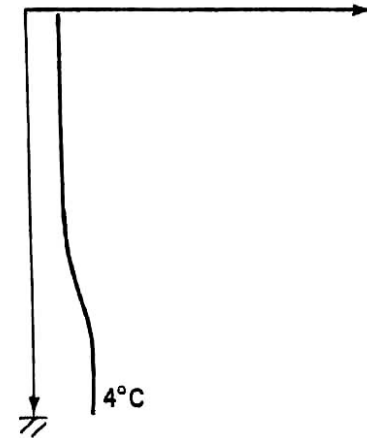


Summer Stratification

(• DO ▲ Temp)

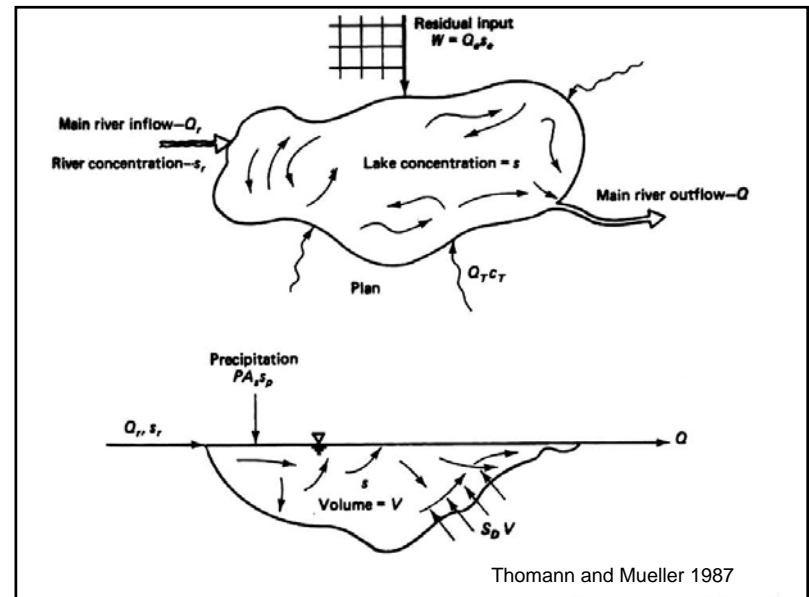
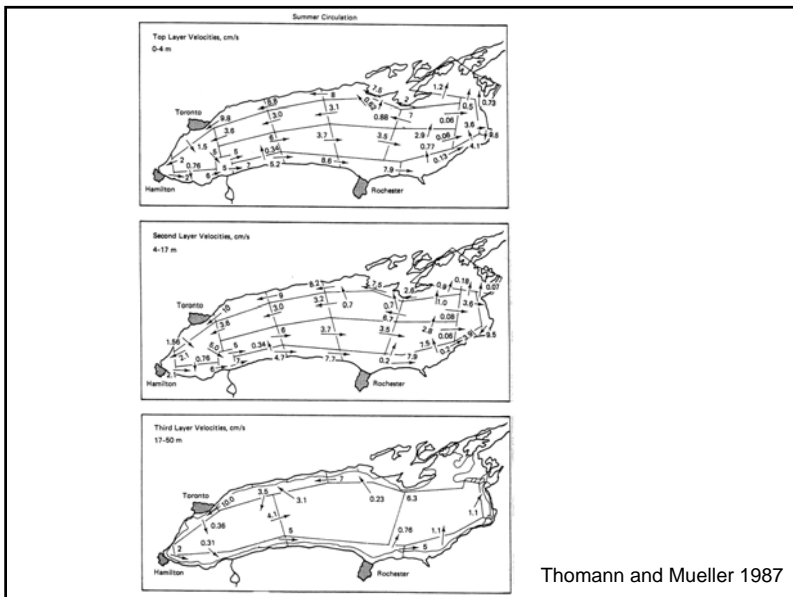
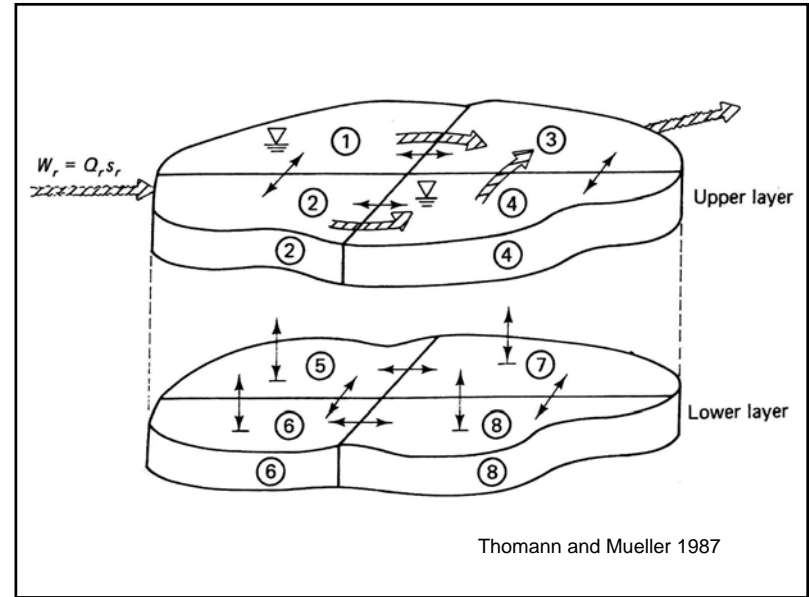
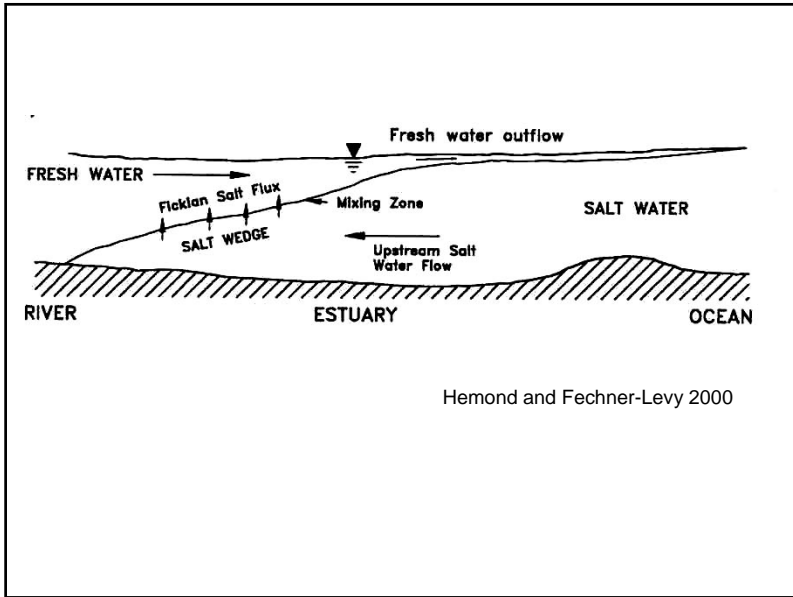


What would lake temperatures look like in winter (very cold area)?



Winter

Thomann and Mueller 1987



$$W = Q_e S_e + Q_r S_r + Q_T S_T + P A_s S_p + S_d V$$

W = mass input [M/T]

Q_eS_e = waste effluent discharged to lake

Q_rS_r = mass from main river

Q_TS_T = mass from tributary

P A_sS_p = mass input from precipitation

S_dV = sediment release

Q_e = effluent discharge

P = precipitation amount

Q_r = river flow

A_s = lake surface area

Q_T = tributary flow

V = lake volume

S_e = effluent concentration

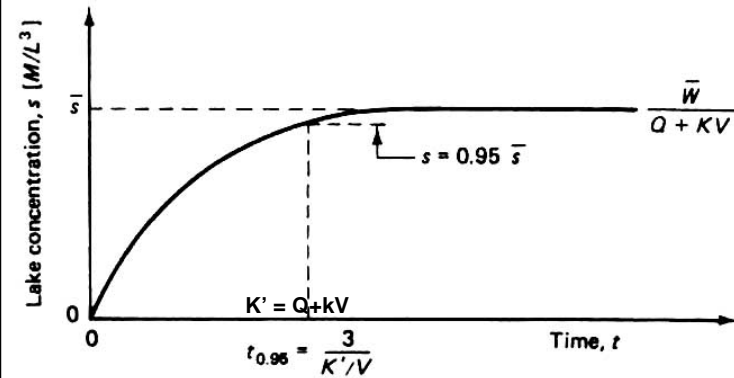
S_r = river concentration

S_T = tributary concentration

S_p = rain concentration

S_d = sediment concentration

Concentration increases with time, since the start of the discharge:



Thomann and Mueller 1987

Concentration Decrease after Discharge Stops

$$\frac{dVs}{dt} = W(t) - Qs - kVs$$

Change of mass with time =
input mass (gain) – mass outflow (loss) – decay (loss)

Assuming a constant Q and k over time

Expanding the derivative:

$$\frac{dVs}{dt} = V \frac{ds}{dt} + s \frac{dV}{dt}$$

If V is temporarily constant: $\frac{dV}{dt} = 0$

$$\text{Then: } \frac{dVs}{dt} = V \frac{ds}{dt}$$

Re-arranging results in:

$$W(t) = V \frac{ds}{dt} + Qs + kVs$$

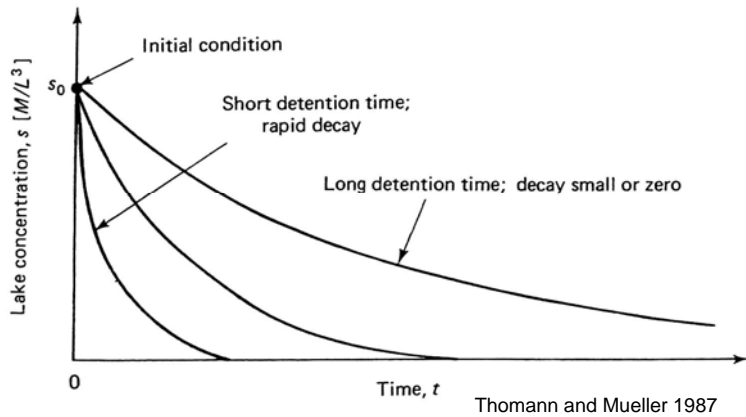
Can simplify if define: $k' = Q + kV$

$$\text{Then: } W(t) = V \frac{ds}{dt} + k's$$

$$\text{Resulting in: } s = s_0 \exp \left[- \left(\frac{1}{t_d} + k \right) t \right]$$

Where the lake detention time, t_d is defined as: $t_d = \frac{V}{Q}$

Concentration decreases from initial conditions (at end of input) by a combination of flushing and decay:

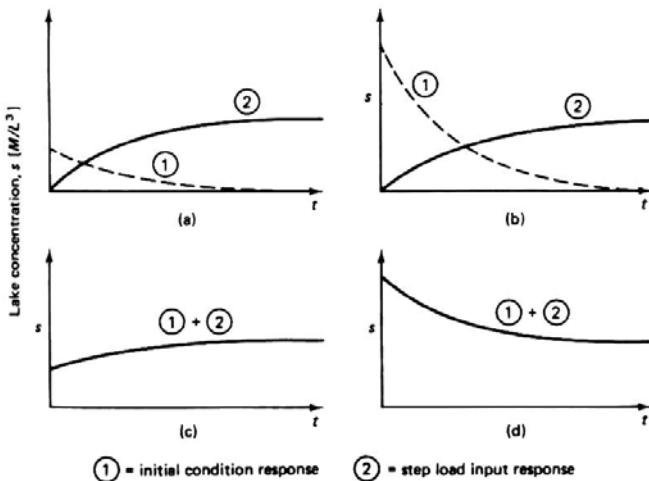


Response due to step load = sum of initial condition (from previous load), plus step load effect:

$$s = \frac{W}{Q + kV} \left\{ 1 - \exp \left[- \left(\frac{Q}{V} + k \right) t \right] \right\} + s_o \exp \left[- \left(\frac{Q}{V} + k \right) t \right]$$

Total response and transitions can be determined by calculating individual responses and summing the effect.

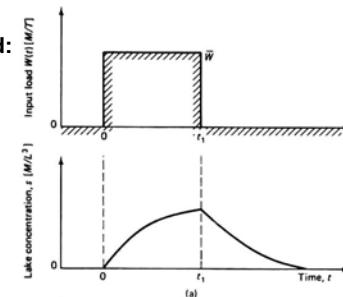
Response due to initial condition and step input. (a) "Small" initial condition. (b) "Large" initial condition. (c) and (d) Sum of components.



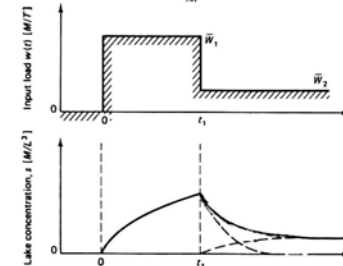
Thomann and Mueller 1987

Response due to varying load:

(a) Step input and subsequent reduction to zero



(b) Step input with reduction to new load level

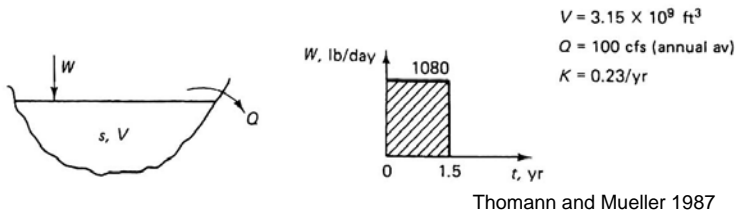


Thomann and Mueller 1987

Example Problem:

A Lake (with initial $s = 0$), receives a load of a slowly reacting pesticide (triallate) of 1080 lb/day for 1.5 years and is then terminated.

1. Determine the equilibrium concentration
2. The maximum concentration
3. The time until a level of 100 $\mu\text{g/L}$ is reached



- (1) Determine the equilibrium concentration

$$\bar{s} = \frac{W}{Q + kV} = \frac{W/Q}{1 + kt_d}$$

$$t_d = \frac{V}{Q} = \frac{3.15 \times 10^9 \text{ ft}^3}{100 \text{ ft}^3/\text{sec}} \times \frac{\text{day}}{86,400 \text{ sec}} \times \frac{\text{year}}{365 \text{ days}} = 1.0 \text{ year}$$

$$\bar{s} = \frac{W/Q}{1 + kt_d} = \frac{1080 \text{ lb/day}}{100 \text{ ft}^3/\text{sec} \times 86,400 \text{ sec/day}} = \frac{0.000102 \text{ lb/ft}^3}{1 + \left(\frac{0.23}{\text{day}}\right)(1.0 \text{ year})}$$

$$\bar{s} = \frac{0.000102 \text{ lb}}{\text{ft}^3} \times \frac{\text{ft}^3}{7.48 \text{ gal}} \times \frac{\text{gal}}{3.78 \text{ L}} \times \frac{454,000 \text{ mg}}{\text{lb}} = 1.63 \text{ mg/L} = 1630 \mu\text{g/L}$$

- (2) Determine the maximum concentration

(the max. concentration will occur at the end of the discharge time, at $t=1.5$ years)

$$s = \bar{s} \left\{ 1 - \exp \left[- \left(1 + kt_d \right) \left(\frac{t}{t_d} \right) \right] \right\}$$

$$s = 1630 \mu\text{g/L} \left\{ 1 - \exp \left[- \left(1 + \frac{0.23}{\text{yr}} 1.0 \text{ yr} \right) \left(\frac{1.5 \text{ yr}}{1.0 \text{ yr}} \right) \right] \right\} = 1370 \mu\text{g/L}$$

Never reaches the equilibrium concentration before it starts to decrease.

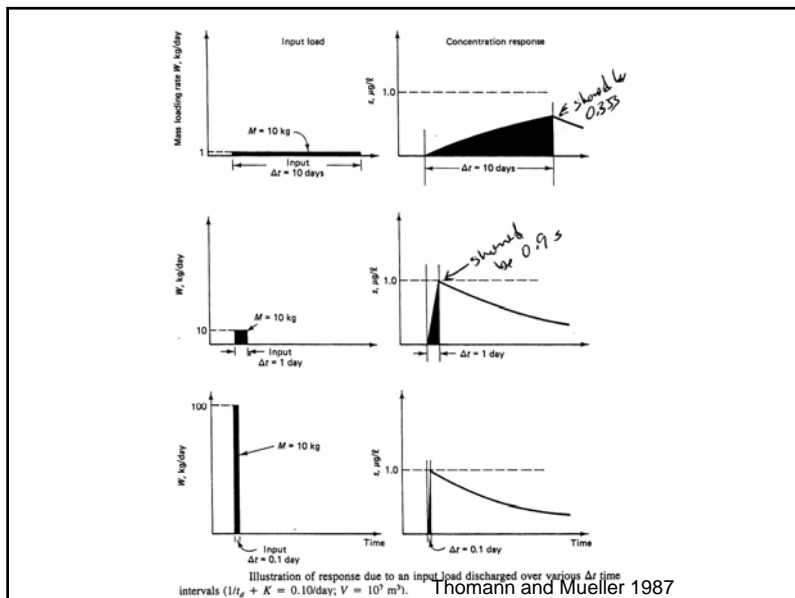
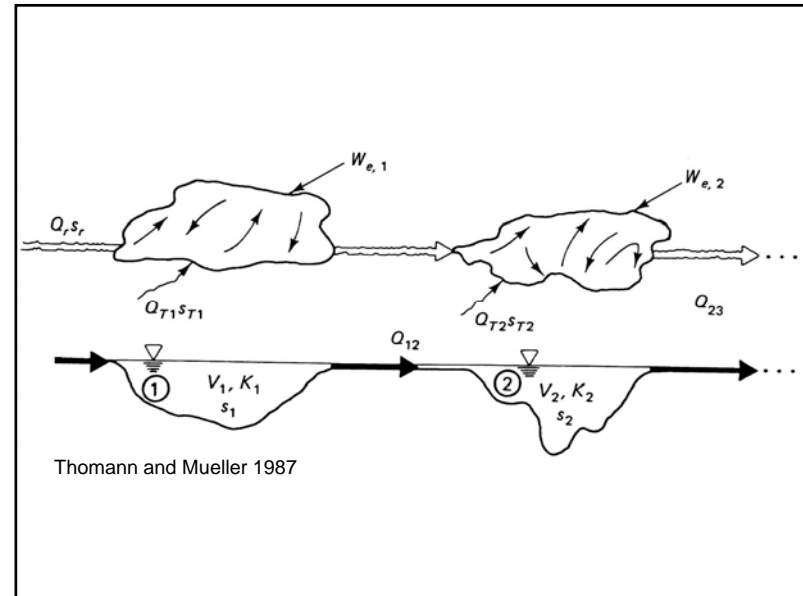
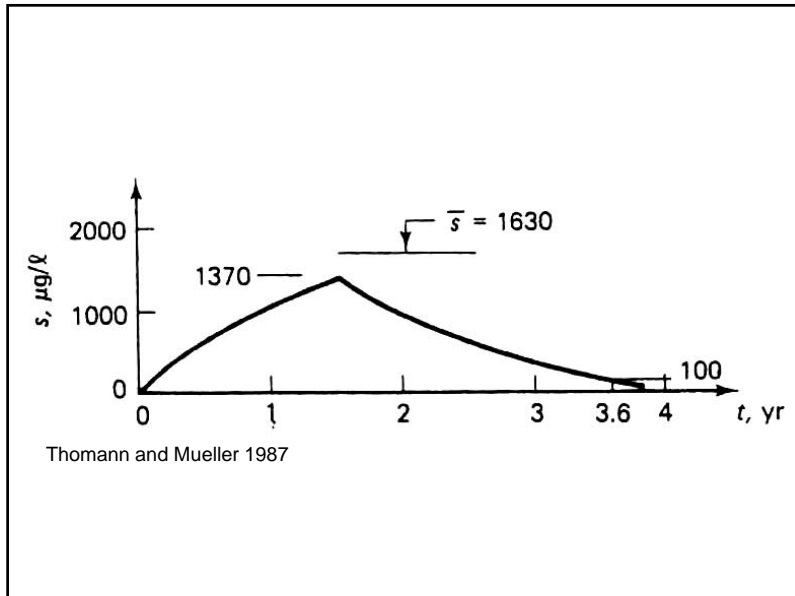
- (3) Determine the time until a level of 100 $\mu\text{g/L}$ is reached

$$s = s_0 \exp \left[- \left(1 + Kt_d \right) \left(\frac{t'}{t_d} \right) \right]$$

Where: $t' = t - 1.5 \text{ years}$

$$100 \mu\text{g/L} = 1370 \mu\text{g/L} \exp \left[- \left(1 + \frac{0.23}{\text{yr}} 1.0 \text{ yr} \right) \left(\frac{t'}{1.0 \text{ yr}} \right) \right]$$

$$t' = 2.13 \text{ years}$$



Movement of Particulates in Natural Water Bodies

Stoke's Law to predict settling of particles (type 1, discrete, non-interacting):

$$\omega_f = \frac{(2/9) \cdot g \cdot (\rho_s / \rho_f - 1) \cdot r^2}{\eta_f}$$

With the sediment and fluid densities, particle size, and kinematic viscosity.

Downward flux due to settling [M/L²T] is therefore:

$$J_{Stokes} = C \cdot \omega_f$$

Corresponding upward flux density:

$$J_{Fickian} = D \cdot dC / dx$$

Vertical concentration profile of particles at steady state:

$$C = C_o \cdot e^{-(\omega_f / D) \cdot x}$$

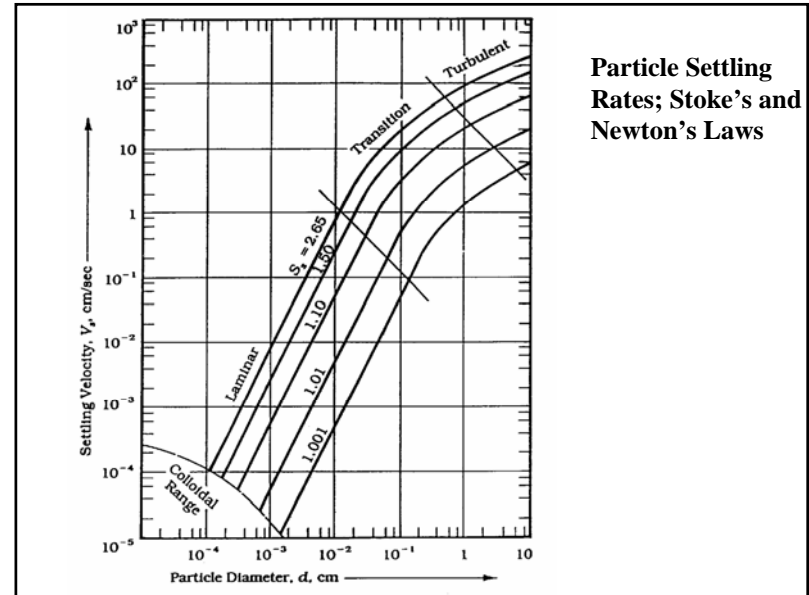
Example 2-3

Describe the steady-state distribution of 1 μm clay particles in still water. Assume kinematic viscosity of water at 50°F is 0.013 cm²/sec and a solid density of 2.6 g/cm³. Also calculate the depth when the concentration is halved.

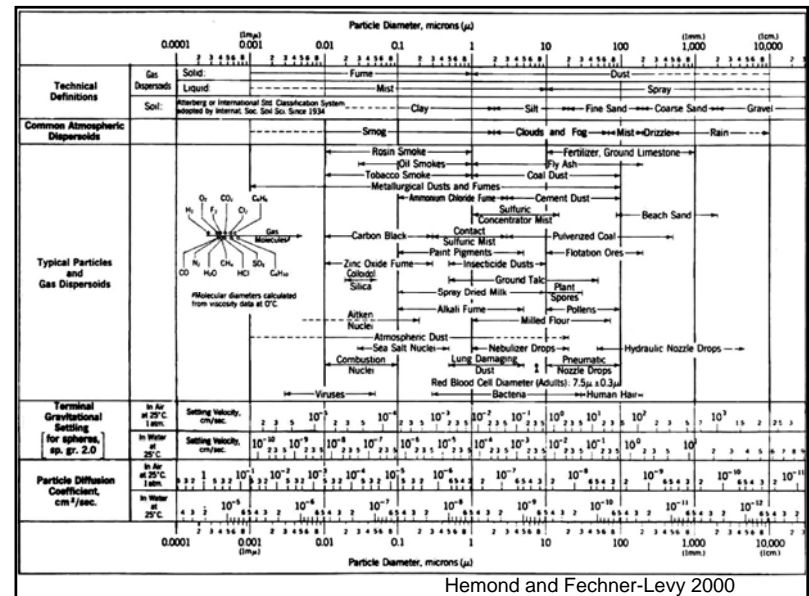
The settling rate for the 1 μm particle is therefore:

$$\omega_f = \frac{(2/9) \cdot g \cdot (\rho_s / \rho_f - 1) \cdot r^2}{\eta_f} = \frac{(2/9) \cdot 981 \text{ cm/sec}^2 \cdot ((2.6 \text{ g/cm}^3) / (1 \text{ g/cm}^3) - 1) \cdot (5 \times 10^{-5} \text{ cm})^2}{0.013 \text{ cm}^2 / \text{sec}}$$

$$= 6.7 \times 10^{-5} \text{ cm/sec}$$



Particle Settling Rates; Stoke's and Newton's Laws



Hemond and Fechner-Levy 2000

The diffusion coefficient for this particle is about $5 \times 10^{-9} \text{ cm}^2/\text{sec}$ (from fig 2-11). The first-order decay coefficient for the large particle is therefore:

$$\omega_f / D = \frac{6.7 \times 10^{-5} \text{ cm/sec}}{5 \times 10^{-9} \text{ cm}^2/\text{sec}} = 1.3 \times 10^4 / \text{cm}$$

The distance at which the concentration is halved is:

$$\frac{1}{2} = e^{-(1.3 \times 10^4 / \text{cm}) \cdot x}$$

$$x = 5 \times 10^{-5} \text{ cm} \text{ or } 0.5 \mu\text{m}$$

Example 2-4

What is the minimum distance the particles will travel before settling to the river bottom? Assume a 2-m river depth and $200 \mu\text{m}$ particles, 2.6 g/cm^3 particle density and $1.3 \times 10^{-2} \text{ cm}^2/\text{sec}$ kinematic viscosity.

Settling rate:

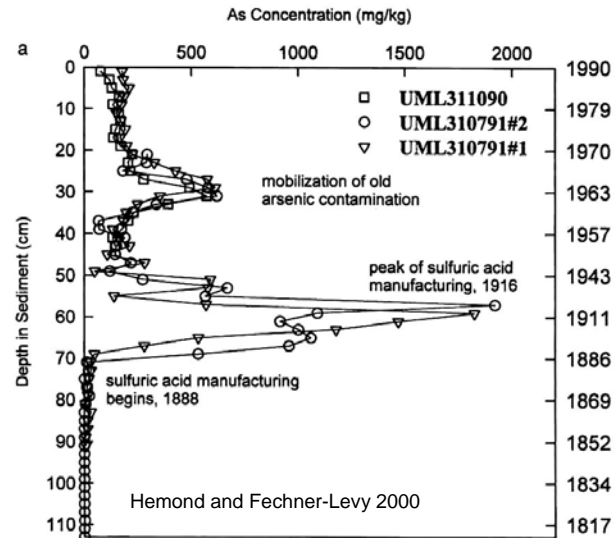
$$\omega_f = \frac{(2/9) \cdot 981 \text{ cm/sec}^2 \cdot ((2.6 \text{ g/cm}^3)/(1 \text{ g/cm}^3) - 1) \cdot (10^{-2} \text{ cm})^2}{0.013 \text{ cm}^2/\text{sec}}$$

$$\omega_f = 2.7 \text{ cm/sec}$$

The time required to settle 2 m is therefore 75 sec, and the particle will travel:

$$75 \text{ sec} \cdot 0.2 \text{ m/sec} = 15 \text{ m}$$

Sediment accumulations:



Example 2-5

Sediment from a 10 cm depth of a lake has a ^{210}Pb activity of 2.5 disintegrations per minute (DPM), while surface sediment has a DPM of 4. How rapidly does sediment accumulate in this lake?

Using the basic equation for radioactive decay:

$$t = \frac{-1}{\lambda} \cdot \ln\left(\frac{A_d}{A_o}\right) = \frac{-1}{0.03/\text{year}} \ln\left(\frac{2.5 \text{ DPM}}{4 \text{ DPM}}\right) = 16/\text{year}$$

$$\frac{10 \text{ cm}}{16 \text{ year}} = 0.6 \text{ cm/year}$$